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## Sustainability and Influencing Factors in Bacterial Cellulose Production: A Review of the Impact of Microorganisms, Culture Media, and Cultivation Methods

## Running title: Advanced Bacterial Cellulose Production

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## SUMMARY

This review offers a comprehensive analysis of bacterial cellulose (BC) production, with a focus on the key factors influencing the bioprocess, including microorganism selection, substrate optimization, and cultivation techniques. It addresses the challenges associated with BC production and proposes strategies for optimizing upstream processes, such as microorganism preservation, inoculum preparation, and culture medium formulation, which are critical for improving production efficiency. Additionally, the review explores the effects of fermentation parameters such as time, temperature, and oxygen availability on BC yield and quality. It also highlights the increasing interest in utilizing alternative substrates, particularly agro-industrial waste, to reduce production costs and enhance sustainability. By evaluating these factors, this review provides valuable insights for advancing BC production in both research and industrial applications.

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# **Keywords:** biocellulose production; oxidative fermentation parameters; microbial selection; bioprocess; agro-industrial waste

## INTRODUCTION

The biotechnology industry produces numerous products derived from microorganism metabolism that benefit humans, animals, and the environment. Among these, bacterial cellulose (BC) has been gaining prominence in industrial applications due to its versatility. BC is a biodegradable, biocompatible biopolymer with high purity, and it is classified as Generally Recognized as Safe (GRAS) by the Food and Drug Administration (FDA) (1-3).

Since its discovery in 1886 during vinegar production, BC has consistently attracted global research interest, with efforts focused on enhancing its production and improving its properties for high-value-added applications (4,5). Potential applications of BC include food additives and dietary fiber-enriched products (6,7), food packaging materials (8), and bioengineering uses such as cell and bioactive compound entrapment, biosensor development (9–11), cosmetics (12), wound dressings (13), and applications in electronics (14). Despite extensive research validating its potential applications, BC's commercial use remains limited due to high production costs. Advancing BC commercialization requires strategies to increase yield and reduce production costs, ultimately making this biopolymer economically viable for broader applications. To achieve this, optimizing microorganism activity, nutrient sources, and fermentation techniques is critical for overcoming these limitations.

From a metabolic perspective, bacterial cellulose is a product of oxidative fermentation by acetic acid bacteria. These microorganisms metabolize carbon sources, such as sugars, ethanol, and sugar alcohols, to produce energy through a series of enzymatic reactions (*15*). Understanding the mechanisms and factors involved in BC formation is crucial for controlling fermentation parameters and optimizing metabolite production. In general, a fermentation process includes three main stages: upstream steps (microorganism selection and preservation, inoculum preparation, and culture medium formulation), the fermentation phase, and downstream steps (product purification and waste management). Each stage directly or indirectly affects product yield, characteristics, bioprocess efficiency, and cost-effectiveness.

Currently, researchers are focusing on isolating new strains with high BC productivity, optimizing culture media, and improving fermentation methods to enhance the efficiency and feasibility of BC production (16-18).

This review provides a comprehensive analysis of the key factors influencing BC production,

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with an emphasis on upstream processes such as microorganism selection and culture medium optimization. Unlike previous studies that focus on isolated aspects of the bioprocess, this review integrates these factors into a detailed discussion of fermentation methods and their critical role in enhancing production yield and cost-effectiveness. This review further highlights the importance of novel microbial strains and advanced fermentation techniques, providing a broader perspective on strategies for enhancing BC production scalability and commercial viability. Additionally, it incorporates recent advances in the use of agro-industrial waste as substrates, aligning with current sustainability trends in biopolymer production.

#### BACTERIAL CELLULOSE

Bacterial cellulose (BC) is an extracellular polysaccharide produced by microorganisms. Unlike plant cellulose, it is a highly pure form of cellulose with a higher degree of crystallinity, which makes it mechanically stronger and more suitable for specialized applications. While plant cellulose is a component of plant cell walls and typically contains impurities such as hemicelluloses and lignin, BC is synthesized in a controlled environment by microorganisms, ensuring superior purity and uniformity (*4*, *19*,*20*).

The first observation of BC dates back to 1886, when Adrian Brown reported the formation of a white, gelatinous film on the surface of the medium during acetic fermentation for vinegar production. At that time, BC was referred to as vinegar-plant or vinegar-mother. Subsequent chemical and structural analyses confirmed its similarity to plant-derived cellulose (*4*, *19*, *20*). Today, BC is also known as biocellulose, microbial cellulose, or bacterial nanocellulose.

The main BC-producing strains belong to acetic acid bacteria (AAB). *Komagataeibacter* genus, due to the higher yields compared to another AAB genera (*21,22*). For microorganisms, BC is a metabolite produced during acetic acid fermentation (oxidative fermentation) that assists in flotation by acting as a cell support at the air-liquid interface. This mechanism, linked to aerobic metabolism, ensures cell survival under stress conditions. In addition, BC helps in cell protection against dehydration, ultraviolet radiation, and acetic acid diffusion to the cytoplasmic membrane (*23–26*). In vinegar production, large volumes of BC might become an issue as they require extra cleaning steps in the fermenters. Also, the presence of AAB in organic vinegar or remaining cells in conventional vinegar (not completely removed by filtration) can affect the visual appearance of the final product (*27*).

However, investigation on chemical composition and structural properties suggested that after purification steps the biopolymer has the potential to produce biotechnological products. Since

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then, researchers have focused on understanding the mechanisms of BC synthesis, isolating BCproducing microorganisms, and optimizing production for controlled processes at both laboratory and industrial scales.

#### Bacterial cellulose-producing microorganisms

Several microorganisms have been identified as producers of BC, such as Aerobacter, Acetobacter, Komagataeibacter, Achromobacter, Agrobacterium, Alcaligenes, Azotobacter, Pseudomonas, Rhizobium and Sarcina (21,22). Among the AAB species, Komagataeibacter xylinus is considered a model for obtaining this biopolymer from different carbon and nitrogen sources due to the high BC yield. However, new species of Komagataeibacter have been continuously isolated for this purpose, including Komagataeibacter medellinensis, Komagataeibacter intermedius, Komagataeibacter hansenii, Komagataeibacter europaeus, and Komagataeibacter rhaeticus (28–31). These microorganisms are usually isolated from Kombucha, fruits, vegetables, and vinegar (32–36). Apart from AAB, new genera and species of microorganisms have been reported as BC producers, for example Bacillus licheniformis (37), Enterobacter sp. FY-07 (38), and Lactobacillus hilgardii IITRKH159 (39).

Bacterial cellulose production is mainly carried out by Gram-negative bacteria, particularly from the genus *Komagataeibacter*, such as *Komagataeibacter xylinus*. These bacteria are efficient BC producers due to their specialized outer membrane and secretion systems, which facilitate the release of cellulose into the extracellular space. Strains like *Komagataeibacter rhaeticus* K3 and *Gluconacetobacter xylinus* have shown high BC yields, often utilizing simple sugars, such as glucose and sucrose. However, the production process requires optimized media and strict environmental control, such as pH and temperature, for maximum efficiency. While Gram-negative bacteria tend to outperform Gram-positive species in BC productivity, the potential of Gram-positive bacteria has recently gained more attention (*40*).

As reported recently by Saleh *et al.* (*40*), Gram-positive bacteria, including *Lactiplantibacillus plantarum* AS.6, *Lactobacillus hilgardii,* and *Bacillus velezensis*, have also demonstrated BC production, though at lower yields compared to Gram-negative strains. The study identified *Lactiplantibacillus plantarum* AS.6 as a promising BC producer with a productivity rate of 56 %, higher than that of other Gram-positive species. When optimized, *L. plantarum* AS.6 can produce 4.51 g/L of BC, doubling the yield compared to the basal medium. This suggests that, with proper optimization of the growth medium, Gram-positive bacteria can be competitive in BC production. Additionally, *L. plantarum* AS.6 produced composites with strong antibacterial activity, indicating its potential for

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#### biomedical applications such as wound dressings and drug delivery.

#### Acetic fermentation and bacterial cellulose synthesis

Bacterial cellulose is an oxidative metabolism product. Acetic acid bacteria obtain energy through the oxidative fermentation (acetic fermentation) pathway to compensate for the low energy yield from aerobic respiration and improve biomass formation through incomplete substrate oxidation (*41,42*). During acetic fermentation, organic substrates such as ethanol, glucose, organic acids, and polyols, are incompletely oxidized to  $CO_2$  and  $H_2O$ . The residual products of this metabolism are utilized in the biotechnology industry to produce high-value-added products (*e.g.* ketones, organic acids, and exopolysaccharides, such as bacterial cellulose) (*43*).

BC biosynthesis is a highly precise and specific process controlled by catalytic and regulatory enzymatic complexes using uridine diphosphate glucose (UDP-Glucose) as a precursor (*44*). In this mechanism, the initial stage is the phosphorylation of glucose to glucose-6-phosphate by the enzyme glucokinase. Then, the phosphoglucomutase promotes the isomerization of glucose-6-phosphate to glucose-1-phosphate, which will be converted to UDP-glucose by uridine diphosphate pyrophosphorylase. The polymerization of glucose into  $\beta$ -glucan chains occurs from UDP-glucose by cellulase synthase, a complex of four subunits, namely bacterial cellulose synthase subunits A; B; C and D, (*BcsA*, *BcsB*, *BcsC*, and *BcsD*), coded by three (*bcsAB*, *bcsC*, and *bcsD*) or four (*bcsA*, *bcsB*, *bcsC*, and *bcsD*) genes. Finally,  $\beta$ -glucan chains are crystallized into cellulose (*22,45,46*).

The synthesized chains are excreted into the medium through pores in the microorganism's cell allowing the elongation and association of the chains in the extracellular medium resulting in BC sub-fibrils (1.5 nm wide). These sub-fibrils give rise to nanofibrils (3–4 nm thick), which ultimately form cellulose ribbons (40–60 nm wide and 3–8 nm thick). The random arrangement of the BC ribbons results in a three-dimensional, porous, and highly crystalline network (*3,4,21,47,48*). The material observed in the culture medium could have different shapes depending on the cultivation method, the strain, and nutrient sources (Fig. 1).

#### Structure, function, and application

As previously mentioned, BC has a structure similar to that of plant-derived cellulose. Cellulose is formed by  $\beta$ -glucopyranosyl units linked by glycosidic bonds  $\beta$ - (1 $\rightarrow$ 4) resulting in a long-chain polymer with a degree of polymerization greater than 20.000 (49). The association between  $\beta$ -glucopyranosyl units originates a planar structure forming a ribbon. This planar and linear structure allows the formation of fibrous and polycrystalline bundles along extensive zones due to the

## association between cellulose molecules by hydrogen bonds. These structures contain both amorphous and crystalline zones (49–51).

In recent years, the production of cellulose from microorganisms has been the subject of research in several countries since the fermentation process originates a material with superior properties and high purity, allowing its application in products such as food, biomedicine, and pharmaceuticals (*16,52,53*). The BC structure formed by the three-dimensional network ensures remarkable properties, namely high mechanical strength, crystallinity, stability to chemical agents and high temperature, high water retention capacity, and resistance to degradability. BC is lignin and hemicellulose-free, nor requiring intense purification, and is also a biocompatible and biodegradable biopolymer (*21,54,55*).

High crystallinity is one of the main characteristics of BC, and the degree of crystallinity ranging from approximately 60 to 90 % depending on the cultivation conditions and strain ability to convert the substrate and adaptation to the fermentation system. Crystallinity influences other characteristics of the biopolymer such as mechanical properties and thermal stability (*34,56,57*). Concerning the crystalline structure, cellulose I (Ia and I $\beta$ ) and cellulose II forms are frequently obtained under fermentation culture. The Ia (triclinic) and I $\beta$  (monoclinic) forms correspond to crystalline structures and differ by the distribution of intra and interunit hydrogen bonds. In cellulose II, the random arrangement of chains results in highly amorphous regions, which also differs by its high thermodynamic stability. In most cases, higher crystallinity is observed in static culture, while amorphous content is more prominent in agitated cultivation (*21,58,59*).

The large surface area, the high number of hydroxyl groups, and its porosity enable BC to interact with water and polymers allowing the application as a support material for enzymes, cell, and nanoparticle immobilization. BC has a high water-holding capacity (WHC), retaining approximately 90% of its weight. This property is due to the strength of the hydrogen bonds involved in the adsorption of water molecules on the surface of the fibers and the density of the bond between the crosslinked fibers. The presence of thin and long ribbons in the BC structure also explains the greater water retention capacity, the moldability and the high tensile strength (30,60-62).

Regarding these characteristics, bacterial cellulose showed potential for food, bioengineering, cosmetics, biomedical, and electronic fields (Table 1 (*7, 19, 46, 63–82*)).

The material can be used in different shapes, for example, nanofibers, nanocrystals, dried or wet pellicles and spheres. In food applications BC acts as a multifunctional ingredient and its addition in food products does not affect sensory characteristics since it can be colored and flavored (69,83). From the nutritional aspect, cellulose has a health-promotion function and can be used as a

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# dietary fiber source, and low calorie or gluten-free products. As food additives these biopolymers have been suggested as a stabilizer, thickener agent and texture modifier (1,3).

The three-dimensional, porous, and crystalline structure added to the presence of hydroxyl groups in the surface area allows BC association to other polysaccharides and proteins by hydrogen, van der Waals, and hydrophilic bonds improving their functionalities. Otherwise, the crystalline structure facilitates hydrophobic interactions, ensuring BC's amphiphilic properties (63,70). The formation of nanocomposites is useful to biodegradable food packaging and edible film development, in this case BC could be associated to other polymers, proteins, bioactive composites, and inorganic nanoparticles to enhance mechanical and thermal properties, barrier performance, and antimicrobial properties (84-86). Some research reports the use of chemical, mechanical, and enzymatic modification to improve or develop specific properties allowing more applications (63-65,87). Besides the several applications fields, the low yield and high production costs are a limiting factor. In this context, it is crucial to understand and optimize the production parameters to improve the cost-effective bioprocess.

Briefly, BC production comprises three stages, (1) upstream, (2) fermentation and (3) downstream. Upstream includes strain selection and conservation, inoculum and medium preparation, and definition of cultivation conditions. During fermentation several parameters can affect the yield and product characteristics, therefore they should be controlled, for example, pH, oxygen, temperature, agitation. Otherwise, downstream steps require the product purification, neutralization, characterization, and effluent treatment. A summary scheme of BC production is shown in Fig. 2.

Various strategies can be employed to overcome or minimize limiting factors at each step of the process, thereby optimizing BC production. The following sections discuss the features of the central factors of BC production (microorganism, substrate, and cultivation methods), including some strategies to improve this bioprocess.

## ACETIC ACID BACTERIA FOR BACTERIAL CELLULOSE PRODUCTION

The cultivation of BC producers is a crucial stage, considering the nutritional requirements for cell metabolism and the microorganism's adaptation to fermentation conditions. In this context, the researchers are constantly trying to find new strains with high capacity to produce BC. AAB strains are fastidious microorganisms to cultivate and isolate, posing challenges for researchers to find alternatives that optimize cell growth and BC production (*88–90*). *Komagataeibacter* species have been previously described as the most efficient in BC production due to their ability to grow and produce BC from different carbon and nitrogen sources (*91,92*). *K. intermediuns, K.rhaeticus, K.* 

*hansenii and K. medellinensis* are frequently referred to highly BC producers, similar to the *K. xylinus* strain, the role-model on BC production. The main sources of BC producers are vinegar (*33,93*), kombucha (*94*), fermented juices (*29*), and fruits and vegetables (*15*).

BC producers have developed mechanisms to survive in stressful conditions, usually like the isolation environment, for example, resistance to high acid and ethanol concentration. All these mechanisms make AAB attractive to industrial processes and are useful to improve the biopolymer formation, extending the rate for bioprocess design (92,95). Also, some *Komagataeibacter* strains presented a remarkable ability to produce BC under alkaline conditions, which could be associated with the protective nature of the material (29,96). Additionally, resistance mechanisms have been investigated at different cultivation, such as static and agitated, and the adaptation to highest rotational speed is referred as a strain-dependent characteristic (91). The cultivation under laboratory conditions and synthetic media can reduce the microorganism resistance suggesting that these mechanisms are inducible or transient (97,98). However, the product formation must be evaluated considering the interaction between strain, culture medium and cultivation conditions. In this case, the same strain cultured in different bioprocesses does not always reproduce the same yield and productivity (Table 2 (17,29-30,56,93,99-102)).

Stress conditions can adversely affect cell metabolism and BC production. These factors may induce spontaneous mutations in cells, resulting in atypical cell morphology and growth, and may also inactivate essential enzymes for polymer synthesis, thus reducing yield and material characteristics (*24, 102*). Besides reducing BC production, the effect of cellulose non-producing cells can be investigated by the polymer structure, and crystallinity is the most affected (*103*). Additionally, the presence of mutant cells influences the fiber assembly process due to the formation of soluble polysaccharides, such as acetan, as both use the same starter molecule, UDP-glucose (*104*). Regarding microorganism activity, it is also important to consider the effects of the cultivation parameters on the emergence of mutant cells. Changes in process parameters, pH, temperature, culture medium volume and oxygen availability affect the cell metabolism and product formation (*105*).

Similarly, stress conditions, such as high sugar concentration, anaerobic conditions, and high temperatures, can induce the viable but non-culturable (VBNC) state, which influences cell monitoring and product formation. Briefly, in VBNC state even if the cells are alive, they do not grow on conventional media (nonselective) used to form colonies. The main affected metabolic and morphologic characteristics are the modification of wall cell components, reduction in respiration rate, nutrient transport, macromolecular synthesis. Nevertheless, cells in VBNC state are more resistant to

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## physical-chemical stress and antibiotics. Modification in the environmental conditions and the media composition could favor the cell growth and reverse this cell state (*41,106,107*).

To improve material formation, BC-producing strains can also be obtained using genetic engineering techniques. Key strategies include modifying the *acs* operon, responsible for cellulose synthesis, and genes like *pgi* and *zwf*, which enhance carbon metabolism to generate BC precursors. Additionally, disrupting competing pathways, such as polyhydroxybutyrate (PHB) synthesis, and regulating cyclic di-GMP levels have shown significant improvements in production efficiency. These modifications leverage advanced synthetic biology techniques to optimize bacterial strains for industrial applications (*108–110*). Yang *et al.* (*111*) developed a recombinant strain for BC production in mannose-rich media by introducing genes from the *Escherichia coli* K-12 strain, which increased BC production on 84 % compared with the wild-type strain. Jacek *et al.* (*112*) modified *K. hansenii* motility and cell size, which are suggested to influence the yield and network organization in BC structure. The use of genetic engineering resulted in thicker ribbons of cellulose arranged in looser networks, and the biopolymer are suggested for scaffold production.

#### Monitoring and control of cell growth

The isolation, cultivation, and cell preservation are crucial steps in bioprocess due to their influence on biopolymer formation. The success of AAB cultivation for bacterial cellulose production has been associated with the nutritional requirements of the microorganism and the cell growth control (27,113).

Culture media for microorganisms are classified based on their composition, such as chemically defined (synthetic), complex, selective, differential, and enrichment media. Using complex medium (composition not exactly known) is a strategy to evaluate the growth characteristics of unknown strains or to create an environment able to supply the complex nutritional requirements of some microorganisms (*114*).

Culture media for AAB isolation, pre-activation, and inoculum propagation are formulated to satisfy nutritional demands, providing components that simulate the characteristics of the isolation environment, such as high-sugar content, acetic acid, and ethanol, which are found in fermentation bioreactors, fruits, vinegar, or fermented beverages—common sources for AAB isolation. The main elements to cell formation are Carbon (C), Nitrogen (N), Hydrogen (H), Oxygen (O), Sulfur (S), And Phosphorus (P) since these components are used in proteins, nucleic acids, carbohydrates, and lipids synthesis (*114*,*115*).

Carbon and nitrogen are the most significant nutrients due to their structural role in various

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cellular components (*17*). Carbon is an essential element to the synthesis of organic components in cell metabolism and energy production. In the culture medium this macronutrient is provided through sugar which represents a large percentage in the formulation. Although AAB can metabolize several carbon sources, ethanol, glucose, mannitol, and glycerol are the most common substrates to these metabolic pathways since they are oxidized by the membrane-bound (periplasmic) dehydrogenases, not requiring previous hydrolysis reaction which would mean an extra cell work. For instance, key dehydrogenases in the oxidative fermentation of carbon sources include pyrroloquinoline quinone-dependent alcohol dehydrogenase (PQQ-ADH) and aldehyde dehydrogenase (ALDH), which oxidize ethanol to acetaldehyde and further to acetic acid, respectively. Additionally, PQQ-dependent glucose dehydrogenase (GLDH) oxidizes polyols to ketones (41,42,116).

Nitrogen is another essential element in the culture medium, required for the production of proteins, enzymes, nucleic acids, and biomass formation. To AAB cultivation and BC production this nutrient may be supplied by organic (yeast extract, peptone, malt extract and amino acids) and inorganic sources, for example, ammonium sulfate ( $(NH_4)_2SO_4$ ) and ammonium nitrate ( $NH_4NO_3$ ) (*17,100,117*).

Also, minerals and vitamins play essential roles in cell growth. Mineral components influence enzyme activity, nitrogen fixation, and electron transfer from substrate to oxygen. Some essential minerals for AAB metabolism are molybdenum (Mo), boron (B) and manganese (Mn). In addition, vitamins such as p-aminobenzoic acid, pyridoxine ( $B_6$ ), cyanocobalamin ( $B_{12}$ ), nicotinamide ( $B_3$ ), and ascorbic acid have shown significant effect on cell growth and BC production (*115,118,119*).

Table 3 (18,33,97,116,120–124) shows the culture medium most used to AAB and its composition. These culture media are mainly formulated by sugar (carbon source) and yeast extract or peptone (nitrogen source). Frequently, additives have been incorporated into culture media to supply the microorganism requirement for nutrients. For example, ethanol has been suggested as an alternative energy source to microorganism growth, also supporting cell recovery from viable but non culturable (VBNC) state and inhibiting the non-producing cells (*34, 125*). Similarly, organic acids such as acetic, citric, malic, lactic, pyruvic, and succinic acid could be metabolized by AAB and used as intermediate metabolites to energy production (*116, 126*).

In addition to media composition, alternative methods can be applied during isolation or enrichment stages in solid media preparation, such as double-layer agar. For AAB strains from industrial vinegar production this method simulates the growth conditions in fermentation tanks (*116*). This technique was described by Entani *et al.* (*120*) and consists in creating an inferior layer with broth

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## with 0.5 % agar. Further, the surface will be coated by the broth with 1.0 % agar. The use of doublelayer agar plate supplies a high humidity environment, for the cells favoring the growing of high-acidity colonies (*116*, *120*).

#### Alternatives to cell enumeration

Estimating the cell population is essential for understanding the microorganism's growth profile, metabolic aspects related to BC production, and fermentation control. The cell growth profile typically consists of four stages: lag, exponential (log), stationary, and death. In the lag phase, cell concentration increases slowly as the microorganism adapts to the cultivation conditions. The exponential growth phase reflects the most intense cell activity and substrate consumption. During the stationary phase, nutrient availability is reduced, and the growth rate equals the death rate. However, cells remain active and continue producing metabolites, such as bacterial cellulose. Finally, the nutrient limitation results in cell death (*127, 128*). Traditionally, the AAB population is determined by cell enumeration in plating or microscopy, and turbidimetric and gravimetric methods. Since these techniques are well established to vinegar and fermented beverages production, they could be applied in BC production to improve the cell growth control and product formation. However, alternative techniques are useful for monitoring cell growth and analyzing microorganism behavior. These methodologies should be applicable to fermentation routine to monitoring cell growth and ensure the bioprocess control.

Plating methods to cultivate and enumerate AAB in synthetic culture media could be affected by the presence of cells in the VBNC which leads to an underestimation of cell count and limits cultivation, isolation and cell maintenance (*116,129,130*). The VBNC state has been associated with discrepancies between the target inoculation rate and plate counting results in fermentation systems. This state can disrupt the direct correlation between biomass formation, substrate consumption, and product yield, as VBNC cells cannot be enumerated (*41,130–132*).

Another limiting factor in cell determination is the attachment of cells to the BC during inoculum propagation and fermentation. During the inoculum preparation on a liquid medium the simultaneous cell growth and BC formation result in the cell holding inside of the biopolymer structure. An alternative to overcome this limitation is the use of cellulase to release cells attached to BC fibers, increasing the number of free cells in the liquid medium and improving cell enumeration (*113,133*).

In addition to growth monitoring, it is crucial to use rapid methods to quantify and identify the cell state (*i.e.* live, dead, or VBNC). Several techniques have been used to quantify both live and dead cells in acetic fermentation. Fluorescence technology has proven useful for this purpose,

showing good results for AAB enumeration compared to the plating method (*113*). Similarly, flow cytometry has been used to assist in cell enumeration during acetic fermentation (*134*) and to assess cell viability after exposure to stress factors (*125*). Additionally, real-time polymerase chain reaction (RT-PCR) offers an alternative to traditional AAB enumeration methods (*12,135*).

#### DESIGNING CULTURE MEDIA TO BACTERIAL CELLULOSE PRODUCTION

Culture media significantly impact the total cost in bacterial cellulose production and require strategies to overcome this limitation and increase the bioprocess economic feasibility (126, 127). The conventional medium used for BC production was developed by Hestrin and Schramm (121). Hestrin-Schramm (HS) composition consists in (%, m/V): glucose (2 %), peptone (0.5 %), yeast extract (0.5 %), anhydrous sodium phosphate (0.27 %), and citric acid (0.115 %). The composition of the culture medium must provide sufficient macro- and micronutrients for cell growth and biopolymer synthesis. Considering the HS composition, each component plays an essential role on microorganism metabolism and BC formation. Carbon is supplied by glucose, which is the ideal precursor for the formation of BC chains (4, 12, 136). Peptone and yeast extract provide amino acids for protein synthesis and essential compounds, such as vitamins and minerals, for microorganism growth (117, 137, 138). Finally, anhydrous sodium phosphate ( $Na_2HPO_4$ ) and citric acid exert a buffering effect during cell cultivation (139).

Increasing BC yield and reducing media costs are essential for bioprocess viability. Nowadays, different approaches have been used to design economically feasible nutrient sources to BC production. These strategies involve modifying individual components of the standard media, supplementing culture media, formulating synthetic media, and using low-cost materials. All approaches must consider an ideal carbon and nitrogen ratio for BC production. In microbial biopolymer production, excess nitrogen increases biomass formation while limiting biopolymer production, whereas an excess of carbon over nitrogen decreases protein synthesis and reduces microorganism growth. Thus, the energy from excess carbon is used to produce the polysaccharide (*28,140,141*).

Many BC studies have reported higher production when HS carbon and nitrogen sources were modified by changing the concentration or the type of the sources. Basu, Vadanan, and Lim (*142*) used response surface methodology to determine the optimal HS composition for the *G. hansenii* strain. In this case, glucose and sucrose were evaluated at different concentrations and the author found higher BC yields with sucrose, a cheaper carbon source compared to glucose. Similarly, Jacek *et al.* (*94*) reported the increase in BC production when replaced glucose by eucalyptus

biomass hydrolysate in HS supplemented with ethanol. Considering N influence on cell growth and biopolymer formation, Santoso *et al.* (*100*) used different nitrogen sources, namely, yeast extract, peptone, malt extract, and ammonium sulfate as substitutes for the nitrogen source in HS composition. The results suggested peptone was the more suitable source for *K. intermedius* (BCRC 910677) while no BC was produced using ammonium sulfate as N substitute.

Synthetic media formulation is another alternative to improve BC yield from different strains. Gomes, Ida and Spinosa (17) evaluated the effect of amino acid supplementation on *K. intermedius* V-05 metabolism for BC production. The authors reported aspartic acid (1.5 g/L), phenylalanine (1.5 g/L), and serine (3.0 g/L) as essential elements on the media formulated (50 g/L sucrose, 10 g/L (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>), 2 g/L Na<sub>2</sub>HPO<sub>4</sub>, 1 g/L MgSO<sub>4</sub>·7H<sub>2</sub>O, and 10 mL/L ethanol) achieving 3.02 g/L from the optimized media.

In recent years, the use of low-cost materials, particularly agro-industrial waste, has gained significant attention for biosynthesis of bacterial cellulose (BC). These materials not only reduce production costs but also contribute to environmental sustainability by utilizing waste that would otherwise be discarded. Several agro-industrial by-products have been successfully used as substrates for BC production, such as cashew apple juice, soybean molasses (*119*), potato peel waste (*143*), sugar beet molasses, cheese whey, tobacco waste (*20*), oat hulls (*144*), and brewing by-products (*e.g.* beer and distillery waste) (*145*).

These waste materials provide a rich source of carbon and nutrients necessary for bacterial growth and BC synthesis. However, their complex and variable compositions present challenges to the fermentation process. The undefined nature of these substrates can lead to inconsistencies in the bioprocess, making it difficult to achieve reproducible results and potentially impacting the quality and yield of the BC produced. For example, the presence of inhibitors or non-fermentable components in these waste materials can hinder bacterial growth or BC production efficiency.

To overcome these challenges, some agro-industrial waste materials require pre-treatment processes such as acid or enzymatic hydrolysis to break down complex polysaccharides and increase the concentration of fermentable sugars. While these treatments can enhance BC production, they also introduce additional costs and can complicate the overall process. Furthermore, extensive purification may be necessary to remove residual contaminants, which further adds to the operational expenses (*114,144*).

Designing an optimal culture medium for BC production requires careful consideration of cost-effectiveness, environmental sustainability, and desired application outcomes. Agro-industrial residues, such as cantaloupe peels (CP) (*146*), starchy kitchen wastes (SKW) (*147*) and paper sludge

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(*148*), have shown great potential as alternative substrates for BC biosynthesis. Enzymatic hydrolysis of these substrates enhances fermentable sugar availability, which significantly boosts BC production. For instance, hydrolyzed CP supported a BC yield of 3.49 g/L, while SKW hydrolysates yielded 2.11 g/L. Similarly, paper sludge enzymatically processed in a fed-batch system increased BC production to 3.10 g/L, outperforming batch fermentation. These results highlight the feasibility of using wastederived substrates to reduce production costs and minimize environmental impact, while offering pathways to valorize cellulosic and starchy wastes (*146–148*).

Optimizing media formulations through techniques such as the Box-Behnken design (BBD) can further enhance BC production and application-specific performance. For instance, BBD optimization of SKW hydrolysis maximized reducing sugar availability, researchers can tailor culture media to achieve sustainable BC production with enhanced functionality for diverse applications, including wastewater treatment, biomedical materials, and environmental remediation (*146–148*).

On the other hand, the use of defined (synthetic) media offers advantages in terms of process control, reproducibility, and scalability. These media have a known and consistent composition, which allows for better monitoring and optimization of fermentation parameters. Additionally, the use of defined media can simplify the recovery and purification steps, leading to higher-quality BC production. However, synthetic media are typically more expensive than agro-industrial wastes, which can offset some of the cost-reduction benefits (*114,144*).

Despite the limitations, the exploration of agro-industrial waste as an alternative culture medium for BC production remains a promising area of research. With further optimization and pre-treatment strategies, agro-industrial by-products can serve as a sustainable and cost-effective source for BC production, contributing positively to both economic and environmental goals. Additionally, BC produced from waste materials could hold higher added value in diverse applications, such as in biocomposites, packaging, and medical products, making it a potential key player in the circular economy (*20,147,149*).

#### **CULTIVATION METHOD**

Bacterial cellulose fermentation can be carried out under static or agitated cultivation, and the method used influences both the yield and material properties. However, the success of each process depends on strain adaptation and the interaction of these variables with the culture medium. Under static conditions, AAB are inoculated into fermentation flasks or bioreactors containing sterile culture medium and incubated at predefined temperature and time conditions. In this method, BC formation occurs at the air-liquid interface as a gelatinous pellicle, shaped according to the flask used

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#### for cultivation (150).

Although static cultivation is the most used technique for BC production, agitated (stirred or shaking) culture has been proposed as an alternative due to its potential to overcome some limitations inherent to the static method. In agitated cultivation, the culture medium inoculated with AAB is incubated under various agitation speeds, and the biopolymer is synthesized as ellipsoidal, stellate, or fibrous components dispersed throughout the culture medium (1). Compared to static cultivation, crystallinity is the most significant characteristic affected by agitation, particularly at high rotation speeds. This parameter reflects the structure organization that would be affected by shear force resulting in a less organized network. Under the agitation system, spherical BC formation results from cell aggregation around air bubbles, following a ribbon-like arrangement. However, the mechanism is also influenced by inoculum, carbon sources, and the temperature of the medium volume (*59,151*).

In their work, Saleh *et al.* (152) reported that BC production is highly influenced by fermentation conditions, with static fermentation consistently outperforming agitated fermentation in terms of yield. Incorporating hydroxyapatite (HA) nanoparticles into the culture medium further enhanced BC production, with static conditions yielding 4.10 g/L, approximately 1.25 times higher than in agitated fermentation. Static fermentation supports BC formation at the air-liquid interface, optimizing oxygen availability, while agitation can cause excessive oxygen diffusion, genetic instability, and reduced yields. Additionally, structural analysis of BC/HA composites confirmed improved functional properties, particularly under static conditions, highlighting their potential in biomedical applications like bone tissue engineering due to enhanced cell viability and attachment (152).

The evaluation of the strain performance under both systems should consider the effect of the culture medium on cell viability and cell ability to adapt the metabolic mechanics under each cultivation method used. Therefore, it is useful to consider the media composition and the strain when comparing the static and agitated methods. The main differences observed in studies comparing both methods, considering the same strain and nutrient sources in both cultivations, include yield, crystallinity index, water retention, porosity, and BC form (Table 4 (24,34,71,103,153)).

These aspects are essential to define the final biopolymer application (*16*,*71*). BC production is influenced by surface area, volume of culture medium, and nutrient availability. Under static cultivation, the surface area-to-volume ratio significantly influences oxygen availability; a larger surface area favors oxygen consumption. Since AAB are aerobic microorganisms, the oxygen supply is essential for cell growth. In this case, cells are suggested to use the BC synthesized, as well as the remaining from inoculum, as a support to access the air–liquid interface improving their oxygen

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# access. In contrast, aeration in the agitated method ensures a greater oxygen supply and improves nutrient availability, thereby enhancing cell growth (*34,103,154,155*).

Despite higher oxygen diffusion under agitation, BC production may be negatively affected by the emergence of mutant cells (non-producing cells), by-product formation, and simultaneous production of water-soluble polysaccharides (WSPS), leading to lower production compared to the static method (*38, 103, 153*). The by-product formation is a consequence of the nutrient consumption, carbon source metabolization and aeration. For example, using glucose as a carbon source Chen *et al.* (*16*) reported higher glucose consumption and gluconic acid production in the shaking system. Krusong *et al.* (*156*) observed gluconic acid formation increased with the aeration rate while BC production and cell content were reduced. Besides these limiting-factors, recent research confirms the ability of some AAB strains to grow and produce BC under agitation, and the yield could be similar or higher than static method (*24,71,103*).

## DOWNSTREAM METHODS OF ISOLATION AND PURIFICATION OF BACTERIAL CELLULOSE

The downstream processes for isolating and purifying bacterial cellulose (BC) can be categorized into three main steps: harvesting, purification, and drying. At the end of the fermentation stage, the produced BC is harvested from the liquid medium and separated using centrifugation or filtration methods (*32,71,153*).

The harvested BC must be purified to remove residues from the culture medium and cells, as these materials can influence the biopolymer's properties, such as crystallinity and color, and may also induce BC contamination (*157,158*). The conventional approach used is alkaline treatment. In this method, BC is purified in an aqueous solution of sodium hydroxide (NaOH) and then neutralized by washing with distilled water. To achieve optimal purification efficiency, literature suggests various combinations of NaOH concentration, temperature, and time. Typically, BC has been purified with 0.1 to 1 M NaOH solution at 80 to 90 °C, for 30 to 60 minutes (*10,17,100*). Alkaline treatment is suggested to be able to remove remaining nutrients from the culture medium and to lyse bacterial cells attached into BC (*102*).

### **BIOPROCESS CONTROL, OPTIMIZATION AND SCALE-UP**

As mentioned, bacterial cellulose has unique properties to industrial applications. However, implementing a highly productive bioprocess is essential to scale up biopolymer production. Each fermentation process can be optimized by using statistical tools to assess the effect of critical parameters on BC production or properties. In addition to the one-factor-at-a-time approach, statistical

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## optimization is often used to define the ideal conditions for BC production by analyzing a wide range of parameters, including the interaction of process variables.

Studies highlight the use of innovative substrates like enzymatically hydrolyzed prickly pear peels (PPP), yielding 6.01 g/L of BC under optimized conditions (68 % PPP substrate, pH 4, 20°C, 11 days). Functionalized BC membranes loaded with fruit byproducts, such as pomegranate peel extract, demonstrated antimicrobial properties and extended the shelf life of strawberries, highlighting their potential in sustainable packaging (*159*).

Statistical models provide time-efficient and cost-effective alternatives for exploring fermentation conditions aimed at large-scale production. Considering their influence on BC yield, the main parameters used in bioprocess optimization include the type and concentration of carbon and nitrogen sources, ethanol, pH, temperature, cultivation method, rotation speed, inoculum concentration, and culture medium volume (*12,32,141,160*).

Statistical optimization techniques, such as Plackett-Burman and Box-Behnken designs, have refined parameters like yeast extract concentration, temperature, and incubation time, significantly enhancing BC yields. For instance, *Gluconacetobacter hansenii* ATCC 23769 achieved 2.91 g/L BC with optimized conditions. Comprehensive characterization of BC membranes revealed high purity, crystallinity, and thermal stability, reinforcing their suitability for diverse applications, from packaging to biomedical and environmental uses (*161*).

Currently, the limitations faced in large-scale implementation are mainly related to raw material costs, energy and water consumption, by-product formation, carbon source metabolism, and the ability to reproduce yields obtained in the initial stages (*105,144*). Scale-up studies and alternatives operation mode have been successfully carried out using different nutrient sources and acetic acid bacteria, confirming that this bioprocess can be more explored to improve BC application (*102,162*).

#### CONCLUSIONS

Bacterial cellulose is a high-value product obtained through acetic acid fermentation and has the potential for widespread use in industrial applications due to its unique characteristics. To achieve this, the key challenge is optimizing the yield to establish a production system capable of meeting industrial demand. Designing a profitable bioprocess requires consideration of the interaction between the three key elements of fermentation: the strain, the culture medium, and the cultivation method. This review aims to present the general aspects of BC production and summarize the main challenges and strategies for increasing production and reducing bioprocess costs. The findings

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presented in this review provide insights into alternatives for improving bacterial cellulose production. Designing bioprocess for bacterial cellulose production requires: 1) a high-productivity strain, either wild-type or genetically engineered; 2) a low-cost nutrient source, achievable using agro-industrial waste or substitution of carbon sources in a synthetic medium; and 3) an optimized cultivation method. An effective combination of these strategies must be explored to ensure bacterial cellulose production and its application at an industrial scale.

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## CONFLICT OF INTEREST

The authors declare that they have no competing interests.

## AUTHORS' CONTRIBUTION

R.P.F. Catarino contributed to the conception of the work, data collection, drafting of the article, and critical revision. V.A.B. Mascareli and A.C.L. Pavanello participated in preparation and revising the manuscript. V.L.P. Costa contributed to the preparation of the paper. W.A. Spinosa was responsible for preparation and revising the manuscript, critical revision and provided final approval of the version to be published.

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Fig. 1. Biosynthesis of bacterial cellulose from glucose and fructose

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Fig. 2. Scheme of bacterial cellulose production

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## Table 1. Bacterial cellulose properties and potential application fields

Application	Function	Structure-propertie	Reference
Meat products; ice cream.	Fat replacer	Water holding capacity; emulsion stabilization;	(63–65)
		amphiphilic nature.	
Dietary fiber source; low calorie	Functional food	Insoluble dietary fiber; high water holding; ion	(7,19,46)
products; low cholesterol diet.	ingredients	exchange capacities.	
Food packaging, edible films and	Food packaging	High surface area; porosity; high pore volume;	
coatings, active and intelligent	and support for	gelling behavior; high crystallinity; hydrophilicity;	(19,66–68)
packaging film; immobilization of cell,	bioactive	rehydration property; chemical, thermal, and	
enzyme, antimicrobial agents	compounds	mechanical stability; barrier properties.	
Pickering emulsion; edible foam;	Thickener and	Amphiphilic nature; high surface area; crystallinity;	(69–75)
beverages; bakery products; dairy	stabilizing agent in	three-dimensional structure.	
products.	emulsion,		
	suspensions, and		
	foam stabilizer		
Bioengineering; tissue engineering;	Controlled release	High purity and crystallinity; porosity;	(76–78)

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	systems;	biocompatibility; nanofibrillar matrix; mechanical	
	biosensors;	strength; durability; flexibility; elasticity	
	scaffold for		
	regeneration;		
	vessel substitute;		
Cosmetics	Bioactive	High water-holding capacity; biocompatibility;	(79)
	compounds delivery	nanofibrillar porous structure;	
Wound dressings; drug delivery	Controlled release	High water absorption capacity; biocompatibility;	(80,81)
systems	systems; water	porosity; crystallinity; thermal stability.	
	retainer		
Electronic field	Flexible substrates for electronic devices, conductive materials, and biosensors	High purity and crystallinity; porosity; biocompatibility; nanofibrillar matrix; mechanical strength; durability; flexibility; large surface area.	(78,82)

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Strain	Source	Nutrient source	Method	Parameter	BC/	BC/	Reference
					(g/L)	(g/(L·h))	
K. europaeus	Rotten	Hestrin Schramm (glucose)	Static	30 ºC/384 h	5.61	0.01	(101)
SGP37	grapes					46	
		Hestrin Schramm	Static	30 ºC/384 h	9.98	0.0260	
		(fructose and ethanol)					
		Sweet lime pulp waste	Static	30 ºC/384 h	6.30	0.0164	(102)
		Sweet lime pulp waste	Static batch	30 ºC/384 h	26.20	0.0682	
		supplemented with HS					
		Sweet lime pulp waste	Static intermittent	30 ºC/384 h	38.00	0.0990	
		supplemented with HS	fed-batch				
K. intermedius	Fermented	Hestrin Schramm	Static	28 ºC/120 h	1.20	0.0100	(29)
BCRC 910677	fruit juice						
		Synthetic optimized	Static	28 ºC/144 h	3.91	0.0271	(100)
		medium					
K. intermedius	Vinegar	Soy molasses with	Static	30 °C/336 h	10	0.0297	(93)
V-05		ethanol					
		Hestrin Schramm	Static	30 °C/336 h	3.7	0.0110	

## Table 2. Acetic acid bacteria performance on bacterial cellulose production under different conditions

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Synthetic with amir	no Static	30 °C/240 h	3.02	0.0125	(17)
acids (optimized)					

(continue)

#### Table 2. – Acetic acid bacteria performance on bacterial cellulose production under different conditions (continued)

Strain	Source	Nutrient source	Method	Parameter	BC/	BC/	Reference
					(g/L)	(g/(L·h))	
K. rhaeticus	Kombucha	Hestrin-Schramm with	Static	28 °C/06 b	6 70	0.0608	(56)
AF-1	tea	ethanol	Static	20 0/9011	0.70	0.0090	(50)
		Cashew tree exudate	Static	28 °C/168 h	2.80	0.0167	(99)
		Cashew gum	Static	28 °C/168 h	2.30	0.0137	
		Hestrin-Schramm	Static	28 °C/168 h	~ 6.0	0.0357	
		HSCTE	Static	28 °C/168 h	~ 6.0	0.0357	
		HSCG	Static	28 °C/168 h	~ 6.0	0.0357	
		Sugarcane molasses-		20 °C/120 h	3.46 -	0.0288 -	( <i>30</i> )
		supplemented	Static	30°C/120 h	4.01	0.0334	
		Sugarcane molasses	Static	30 °C /120 h	1.90	0.0158	
		Hestrin Schramm	Static	30 °C/120 h	3.00	0.0250	

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Culture media	Composition	Function	Reference
AE	1.5 % glucose; 0.2 % yeast extract; 0.3 %	Isolation and enrichment	(120)
	peptone; 2.0 % ethanol; 6.5 % acetic acid.		
Glucose-yeast extract-	10 % glucose; 1.0 % yeast extract;	Isolation and enrichment	(97)
carbonate (GYC)	2.0 % CaCO <sub>3.</sub>		
Hestrin-Schramm (HS)	2.0 % glucose; 0.5 % yeast extract; 0.5 %	Isolation, cultivation, and bacterial	(18,33,116,121)
	peptone; 0.27 % Na <sub>2</sub> HPO <sub>4</sub> ; 0.115 % citric	cellulose production	
	acid.		
Mannitol, yeast extract,	2.5 % mannitol; 0.5 % yeast extract; 0.3 %	Isolation and enrichment	(116)
peptone (MYP)	peptone.	Preservation	
Carr	2.5 % yeast extract; 2.0 % ethanol; 0.02 %	Preservation	(122)
	peptone.		
Glycerol	15 % glycerol	Preservation	( <i>123</i> )
Malt extract	20 % malt extract	Preservation	(124)

### Table 3. Main culture media for acetic acid bacteria isolation, cultivation, and preservation

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Strain	Static/	Agitated/	BC properties	BC properties	Reference
	(g/L)	(g/L)	Static	Agitated	
A. xylinum BCA263	3.97	1.70	Higher crystallinity;	Larger porous; lower	(71)
K. xylinus BCC529	2.48	1.66	stronger tensile strength;	crystallinity; higher water	
G. xylinus P1	1.40	1.72	denser network structure; higher temperature resistance.	retention.	
K. xylinus (KX)	1.14–1.84	0.60 - 1.20 (~)	Higher crystallinity and	Disorderly reticulated	(103)
K. xylinus (TISTR 086)	0.14–0.39	0.00 - 0.10 (~)	smaller crystallite sizes;	structures of microfibrils;	
K. xylinus (428)	0.09–0.22	0.20 - 0.40 (~)		higher cellulose I $\alpha$ content in	
K. xylinus (975)	1.11–1.55	(~) 2.40 - 3.54		the flocky asterisk-like BC	
K. xylinus (1011)	0.57–1.46	(~) 3.20 - 4.69		than in the solid sphere-like.	
Komagataeibacter sp.	8.85	3.22	Higher crystallinity; high	Network structure looser and	(153)
nov. CGMCC 17276			water-holding capacity;	more porous; higher porosity.	
			denser network.		
			Thicker fibers; higher	Higher weight loss; higher	
K. hansenii JR-02	4.62	3.14	thermal degradation	moisture content and	(34)
			temperature and lower	amorphous proportion.	

## Table 4. Bacterial cellulose production by acetic acid strains under static and agitated cultivation

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r	moisture content; higher
C	crystallinity.

lable 4 – Bacterial cellulose production by acetic acid strains under static and agitated cultivation (continued	Table 4 – Bacteria	I cellulose production	by acetic acid strains	under static and agitated	cultivation (continued)
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Strain	Static	Agitated	BC properties	BC properties	Reference
	g/L	g/L	Static	Agitated	
			Ordered and dense	Slight decrease in the	
			network of fibrils with (8-	crystallinity index; looser	
			10 nm diameter); the	clump of disordered short	
G. hansenii P2A	1.89	3.25	network was composed of	and thin fibrils; lower	(24)
			interconnected layers.	molecular weights; increased	
				thermal due the gradual	
				increase in I $\beta$ phase content.	